Residual Gas in the LIGO Beam Tubes: Science, Arts and Recipes

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> > LIGO-G030701-00-Z



Interferometers

international network

Simultaneously detect signal (within msec)



LIGO Observatory Facilities



LIGO Hanford Observatory [LHO]

26 km north of Richland, WA

2 km + 4 km interferometers in same vacuum envelope

LIGO Livingston Observatory [LLO]

42 km east of Baton Rouge, LA Single 4 km interferometer

Beam Tubes and Enclosures

Precast concrete enclosure





- Beam Tube
 - 1.2m diam; 3 mm stainless
 - special low-hydrogen steel process
 - 65 ft spiral weld sections
 - 50 km of weld (NO LEAKS!)
 - In situ 160 C bakeout
 - 20,000 m³ @ 10⁻⁸ to 10⁻⁹ torr



LIGO

vacuum equipment



LIGO-G000306-00-M



HOVE_SITE_OVERVIEW

HOVE_SITE_OVERVIEW.adl



THU OCT 30 07:49:09

	PRAXAIR TA	١K		
7	Identities			
.00 IP-12	Praxair numbers all start with 85143XX			
	CP#	Praxair #		
	EY CP7	71		
BSC9	MY CP4	72		
	MY CP3	74		
GV20	LY CP1	75		
4 PT-510	LX CP2	76		
04 4,98e-04 09 1,45e-09	MX CP5	77		
	MX CP6	79		
	MX CP8	80		

LIGO Beam Tubes

• Interaction region between gravitational waves and laser interferometers

- >> 16 km of vacuum tubing at two sites
- >> initial detectors require 10⁻⁷ torr
- >> ultimate detectors require 10⁻¹⁰ torr
- >> needs to be economical
 - minimal pumping, exploit passive nature of system
 - new welding techniques continuous spiral weld in 304L

 low outgassing materials - air bake to reduce hydrogen outgassing, total low 150C bake to reduce water and heavier molecule outgassing

- mass production cleaning
- global positioning system alignment

BEAM TUBE SCIENTIFIC REQUIREMENTS

VACUUM REQUIREMENTS

- >> Residual gas
 - Leak requirements
- >> Contamination
- >> Operational requirements
 - Pump down time
 - Isolation from chambers
 - Reliability

MECHANICAL AND OPTICAL REQUIREMENTS

>> Clear Aperture

- >> Forward and Backscatter from walls and baffles
- >> Motion of tube walls and baffles

BEAM TUBE REQUIREMENTS

• LEAK LIMITS

>>Component Level

 -1 x 10⁻¹⁰ torr liters/sec
 >>2 km module with 2500 liter/sec end pumps
 -1 x 10⁻⁹ torr liters/sec

 CONTAMINATION ON OPTICS

 >> less than 1 monolayer of hydrocarbon/month

BEAM TUBE REQUIREMENTS

OPERATIONAL REQUIREMENTS

- >> Time to reach required pressure < 2 months
- >> Capability to isolate beamtubes from chambers
- >> Reliability: leak free state for > 20 years

MECHANICAL AND OPTICAL REQUIREMENTS

>> Unobstructed aperture 1 meter

>> Backscatter from baffles and tube between 0.5 to 1 micron wavelengths $< 2 \times 10^{-3} \text{ sr}^{-1}$ for angles of incidence greater than 45 degrees

>> Motion of tubes at baffles not to exceed 2 x the ambient seismic noise except in narrow bands

Beam Tube Properties

module length	2 km
25 cm diameter pump ports/module	9
radius of beam tube	62 cm
volume of module	4.831 x 10 ⁶ liters
area of module	$1.55 \text{ x } 10^8 \text{ cm}^2$
initial pumping speed/surface area	$1.94 \text{ x } 10^{-5} \text{ liters/sec/cm}^2$
length/short section	1.90 x 10 ³ cm
wall thickness	$3.23 \times 10^{-1} \text{ cm}$
stiffener ring spacing	76 cm
stiffening ring width	$4.76 \ge 10^{-1} \text{ cm}$
stiffening ring height	4.45 cm
expansion joint wall thickness	$2.67 \text{ x } 10^{-1} \text{ cm}$
expansion joint convolutions	9
expansion joint longitudinal spring rate	1.5 x 10 ⁹ dynes/cm

Initial Interferometer Noise Budget



Advanced Interferometer Noise Budget





BEAM TUBE BAKEOUT

Requirements and goals

>> Initial interferometer residual gas phase noise (100Hz)

 $h(f) < 5 \times 10^{-24}$

>> Advanced interferometer residual gas phase noise (100Hz)

 $h(f) < 1.5 \times 10^{-25}$

>> Relation bewteen pressure and phase noise

$$h(f) = 4.8 \times 10^{-21} R\left(\frac{x}{H_2}\right) \sqrt{\langle P(torr) \rangle_L}$$

BEAM TUBE BAKEOUT

Gas Species	$R(x/H_2)$	Requirement (torr)	Goal (torr)
H ₂	1.0	1×10 ⁻⁶	1×10 ⁻⁹
H ₂ O	3.3	1×10 ⁻⁷	1×10 ⁻¹⁰
N ₂	4.2	6×10 ⁻⁸	6×10 ⁻¹¹
СО	4.6	5×10 ⁻⁸	5×10 ⁻¹¹
CO ₂	7.1	2×10 ⁻⁸	2×10 ⁻¹¹
CH ₄	5.4	3×10 ⁻⁸	3×10 ⁻¹¹
AMU 100 hydrocarbon	38.4	7.3×10 ⁻¹⁰	7×10 ⁻¹³
AMU 200 hydrocarbon	88.8	1.4x10 ⁻¹⁰	1.4x10 ⁻¹³
AMU 300 hydrocarbon	146	5×10 ⁻¹¹	5×10 ⁻¹⁴
AMU 400 hydrocarbon	208	2.5x10 ⁻¹¹	2.5x10 ⁻¹⁴
AMU 500 hydrocarbon	277	1.4×10 ⁻¹¹	1.4×10 ⁻¹⁴
AMU 600 hydrocarbon	345	9.0x10 ⁻¹²	9.0x10 ⁻¹⁵

Table 1: Residual gas phase noise factor and average pressure

BEAM TUBE BAKEOUT

• Average pressure and outgassing rate

$$\langle p \rangle_L = J \left[\frac{2\pi aL}{nF} + \frac{L^2}{4\nu a^2(n-1)^2} \right]$$

Outgassing rate vs temperature and time

$$J(T) = ae^{-\frac{T_0}{T}}$$

>> Typical: $5000 < T_0 < 10000 K$

>> Time dependence

- 1 /t surface adsorption with distribution of binding site energies

- (1/t)^{0.5} diffusion followed by evaporation





Leak pressure profiles in tube



Leak localization algorithm

Beam Tube Cleaning

Cleaning steps

>> Hot water and detergent - Mirachem 500 spray wash

- 30/1 water/Mirachem - 500

-1 cc/ cm²

>> Steam rinse

- -2 cc/ cm²
- 7 8.5 atmospheres pressure
- 58 65 C surface temperature of steel

>> Applied by rotating wand that traverses the tube longitudinally at 20 cm / minute

Surface analysis

>> Fourier Transform Infrared Spectroscopy FTIR

Sample taken by pouring 2 - isopropanol in strip down tube

- Analysis made in professional testing laboratory

Beam Tube Cleaning

>> Auger electron spectroscopy

- Sample strips placed in tube

 Analysis made in surface measurement lab after cleaning

- Sensitive to elemental carbon

Useful to determine state of rinse by measurement of sodium and calcium

>>Water drop adhesion tests

- Qualitative but can be made on location

- Useful in diagnosis of oil layers (poor adhesion) and incomplete rinse of detergent (super adhesion and wetting).

FTIR absorption at 2950 cm--1 CH stretch band normalized : Sat Apr 5 11:35:58 1997





$$z = \frac{(\ln(I/I_0)_{\text{sample}} - \ln(I/I_0)_{\text{reference}}) \times \text{KBr area} \times \text{sample volume in tube}}{\text{sample volume evaporated on KBr} \times \text{area of tube exposed}}$$

Typical values:

Area of tube exposed $= 2 \times 10^4 \text{ cm}^2$ Sample volume in tube = 2 liters Sample evaporated = 200 ccKBr area $= 0.6 \text{ cm}^2$

 $z \approx 1 \times 10^{-4}$ corresponds to 0.1 monolayer of 100 amu hydrocarbon



Spectra of tube B-005 uncleaned, and cleaned with sample taken along and off the drain line. The off drain sample is more characteristic of the average wall condition. The spectra have had the reference spectrum of the isopropanol subtracted, hence the negative values of the absorption.

tube # or surface	condition	0 min	1 min	2 min	3 min	4 min
22B	uncl	57.4	24.3	16.5	11.8	10.8
22B	cl	26.1	8.1	6.5	4.4	5.1
B-005	uncl	59.5	17.6	10.6	8.3	7.1±1.0
B-005	cl 1	24.3	5.2	2.3	1.0±1.0	0.0±1.0
B-005	cl 2	21.9	6.7	2.1	1.0±1.0	0.0±1.0
Oxidized	super cl	35.1	22.1	3.0	2.7±1.0	2.4±1.0
smooth	super cl	27.9	2.9	0.0±1.0		
rough	oily	61.9	64.9	63.2	62.3	62.3

Table 1: Auger analysis 270 ev Carbon line given in terms of 10^3 counts in 1.64 minutes vs A^+ milling time

Conditions:

Incident electron energy = 5kVIncident electron current = 100nAIon milling energy = 2kVIon current density = $10\mu A/cm^2$

 $5 \ge 10^4$ counts of 270 ev electrons in 1.64 sec of acquisition time corresponds to 1 monolayer of carbon bearing molecule

Hydrogen Reduction

- Dry air bake at 454C for 36 hours
 - Reduced 1 micron reflectivity of 304 L
 - Max temperature to minimize Carbide formation
- Mechanism:
 - tight (20000K) and loose (5000K) H binding sites
 - reduce density of loosely bound H and J(300K)
 - surface important for recombination (Myers)
 - Oxide layer not a significant factor
- Avoid reintroduction in welding
 - Dry purge gas until weld is cool
 - Clean weld rod





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t(s)

H2 outgassing after vacuum bake vs H2 outgassing pre bake : Thu Mar 25 19:25:27 1993







Chromium Carbide formation boundary temperature vs time at temperature From several sources



Carbide Precipitation Boundary 304 SS .038 - .03% Carbon : Wed Mar $\ 9 \ 23:04:48 \ 1994$

Heuristic Statistical Mechanics Model

Dubinin-Radushkevich (DR) equilibrium surface coverage:

$$\frac{\sigma}{\sigma_m} = e^{-(T/T_0)^2 ln^2 (P/P_0)}$$

DR site distribution function:

$$\theta(T_{bind}) = (2T_{bind}/T_0^2)e^{-(T_{bind}/T_0)^2}$$
$$\int_0^\infty \theta(T_{bind})\delta T_{bind} = 1$$

Heuristic surface potential:



Emission time:

$$\tau_{emit}(T_{bind}) = \tau_0 e^{T_{bind}/T}$$

Adsorption time:

$$\tau_{ads} = \frac{4n\sigma_0}{\alpha \rho v_{th} (1 + (1 - R)T_{bind}/T) e^{-(1 - R)T_{bind}/T}}$$

Detailed balance per site:

$$\frac{dP(T_{bind},t)}{dt} = -\frac{P(T_{bind},t)}{\tau_{emit}} + \frac{(1 - P(T_{bind},t))}{\tau_{ads}}$$

Integration:

$$P(T_{bind},t) = P(T_{bind},0)e^{-t/\tau} + P_{equil}(T_{bind})(1 - e^{-t/\tau})$$

where

$$\tau = \frac{\tau_{emit}\tau_{ads}}{(\tau_{emit} + \tau_{ads})}$$

and

$$P_{equil}(T_{bind}) = \frac{\tau_{emit}}{(\tau_{emit} + \tau_{ads})}.$$

Incremental outgassing rate of band of sites:

$$dJ_{out}(t) = n\sigma_0 \ \theta(T_{bind})(\frac{dP(T_{bind}, t)}{dt}) \ \delta T_{bind}$$

Aside: for $P(T_{bind}, 0) = 1$ and $\tau_{ads} \to \infty$

$$J_{out}(t,T) = \left(\frac{2n\sigma_0 T}{tT_0}\right) \int_0^a bln(y/a) e^{-(bln(y/a))^2} e^{-y} dy$$

where

$$b = T/T_0$$
 $a = t/\tau_0$

Computational algorithm (waterbakesm.f)

Step time:

$$\Delta t/\tau_s = f \quad \tau_s = V/F$$

Probability computation over 1024 binding energies $0 \rightarrow 3T_0$

 $P(T_{bind}, t_{j+1}) = P(T_{bind}, t_j) e^{-f\tau_s/\tau_j} + P_{equil}(T_{bind}, t_j) (1 - e^{-f\tau_s/\tau_j})$

Surface coverage:

$$\sigma(t_{j+1}) = n\sigma_0 \sum_{0}^{3T_0} \theta(T_{bind}) P(T_{bind}, t_{j+1}).$$

Outgassing rate:

$$J(t_{j+1}) = \frac{(\sigma(t_{j+1}) - \sigma(t_j))}{f\tau_s}$$

Pressure:

$$p(t_{j+1}) = p(t_j) e^{-f} + (\frac{J(t_j)A}{F})(1 - e^{-f})$$

GO BACK AND DO IT AGAIN (new time and temperatures)







btdpumpdwn7b.txt T0=1.0e4 sigma0=150.0 r=0.7 : Thu Aug 8 19:04:00 1991



BEAM TUBE BAKEOUT ELECTRICAL HEATING POWER





SCHEMATIC OF PUMPS AND RGA DURING BAKEOUT





POST-BAKE TEST CONFIGURATION





CALIBRATION ASSEMBLY

LEGEND:















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Postbake measurements of module X1 at Hanford

March 11-12, 1999

Table 1: Results from gas model solution of 16.9 hour postbake accumulation ending March12, 1999 at 10:00AM .

molecule	Outgassing rate @ 10C	pressure@ 10C	outgassing rate @ 23C	pressure@ 23C
	torr liters/sec/cm ²	torr	torr liters/sec/cm ²	torr
H ₂	1.6 x10 ⁻¹⁴	1.0 x 10 ⁻⁹	5.2 x10 ⁻¹⁴	3.4 x 10 ⁻⁹
CH ₄	$< 2 \text{ x } 10^{-20}$	< 3.4 x 10 ⁻¹³	< 8.8 x 10 ⁻²⁰	< 1.5 x 10 ⁻¹²
H ₂ O	< 3 x 10 ⁻¹⁹	< 5.2 x 10 ⁻¹³	< 1.3 x 10 ⁻¹⁸	< 2.3 x 10 ⁻¹²
N ₂	$< 9 \ge 10^{-19} $	< 1.5x 10 ⁻¹³		
СО	< 1.3 x 10 ⁻¹⁸	< 1.7 x 10 ⁻¹³	< 5.7 x 10 ⁻¹⁸	< 7 x 10 ⁻¹³
O ₂	< 1.2 x 10 ⁻²⁰	< 2.3 x 10 ⁻¹⁴		
А	< 2.5x 10 ⁻²⁰	< 3.6 x 10 ⁻¹⁴		
CO ₂	< 6.5 x 10 ⁻²⁰	< 1.2x 10 ⁻¹³	< 2.9 x 10 ⁻¹⁹	<5.2 x 10 ⁻¹³
NO+C ₂ H ₆	< 1.5 x 10 ⁻¹⁹	< 1.6 x 10 ⁻¹³	< 6.6x 10 ⁻¹⁹	< 7.2 x 10 ⁻¹³
H _n C _p O _q	$\sum_{< 1.2 \text{ x } 10^{-19}} \text{amu41,43,55,57}$	< 2.2 x 10 ⁻¹³	$\sum_{< 5.3 \text{ x } 10^{-19}} \text{amu41,43,55,57}$	< 9.7 x 10 ⁻¹³

Volume = 2.4×10^6 liters and Area = 7.8×10^7 cm²

** The equivalent air leak into the module $Q < 3.5 \times 10^{-11}$ torr liters/sec from amu 28.

Correction from 10C to 23C uses a binding temperature of 8000K for hydrogen and 10000K for all other molecules

The data shows the outgassing rates of the tube are acceptable. The higher temperature bake at 168C for a shorter time has accomplished a better result than the longer bakes at 150C.

Beam Tube Bakeout Results

	Outgassing Rate corrected to 23 °C torr liters/sec/cm ² (All except H ₂ are upper limits)					
molecule	Goal*	HY2	HY1	HX1	HX2	
H ₂	4.7	4.8	6.3	5.2	4.6	× 10 ⁻¹⁴
CH ₄	48000	< 900	< 220	< 8.8	< 95	× 10 ⁻²⁰
H ₂ O	1500	< 4	< 20	< 1.8	< 0.8	× 10 ⁻¹⁸
СО	650	< 14	< 9	< 5.7	< 2	× 10 ⁻¹⁸
CO ₂	2200	< 40	< 18	< 2.9	< 8.5	× 10 ⁻¹⁹
NO+C ₂ H ₆	7000	< 2	< 14	< 6.6	< 1.0	× 10 ⁻¹⁹
H _n C _p O _q	50–2 [†]	< 15	< 8.5	< 5.3	< 0.4	×10 ⁻¹⁹

air leak 1000 < 20

*Goal: maximum outgassing to achieve pressure equivalent to 10⁻⁹ torr H₂ using only pumps at stations [†]Goal for hydrocarbons depends on weight of parent molecule; range given corresponds with 100–300 AMU